# **Heat Transfer Enhancement: Pulsatile Flow**

(B. Chehroudi and M. Ghiassian)





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The convection heat transfer coefficient can also be increased by *inducing pulsating flow* by pulse generators, by inducing swirl by inserting a twisted tape into the tube, or by inducing secondary flows by coiling the tube.

B. Chehroudi, PhD



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IN THIS note, a simple approximate analysis of the onstant heat flux boundary condition is presented with the asumption that the fluid enters the tube with a constant velocity nd temperature. For the developed velocity profile, we may write

$$\frac{u}{v_{*}} = 2(2y^{*} - y^{*2}) \qquad (1)$$

(2)

(3)

(4)

or a developing profile, Schiller assumed<sup>2</sup>

$$\frac{u}{U} = 2\frac{y}{\delta^*} - \frac{y}{\delta^{*2}} \quad \text{for} \quad \delta^* \le 1$$

From the continuity of flow, it follows

wight Heat Transfer in the Inlet To Eniformly Heated Tube

B, D = inside radius and diameter of the tube x, y = position coordinates as shown in Fig. 1.

 $\delta_{R} = dimensionless velocity boundary-layer thickness$ 

 $\delta_{\rm s} \delta_{\rm s}/R$  = dimensionless thermal boundary layer-thickness

U/no = dimensionless velocity outside boundary layer

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y/R =dimensionless distance from the wall 5.5. = velocity and thermal boundary-layer thickness in

ut u = inlet and z-component of velocity

U = velocity outside boundary layer

in the = inlet, fluid, and wall temperatures

Fig. 1

= Prandtl number

= Reynolds number

c = boundary heat flux

ters, September 10, 1964.

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Pr= ----

1:4D

$$\delta^* = 2\sqrt{6/U^* - 2}$$

Further, from momentum considerations, Schiller gives the relation:

$$\frac{x}{D \operatorname{Re}} = \frac{1}{80} \left[ 24 - \frac{37}{\sqrt{2}} \sin^{-1} \frac{1}{3} + \frac{58}{3} U^* - 22 \ln U^* \right. \\ \left. - \frac{17}{3} U^* \sqrt{6/U^* - 2} - 16 \sqrt{6/U^* - 2} \right. \\ \left. - \frac{37}{\sqrt{2}} \sin^{-1} \left( \frac{2}{3} U^* - 1 \right)^2 \right]$$

For a temperature solution, the following regions, as in Fig. 1, are considered separately: Region A, from entrance to distance  $x_{k}$  where velocity and thermal boundary-layer development is in progress; Region B, from  $x_k$  to  $x_i$  where velocity profile is fully developed but thermal boundary-layer development is still in progress; and Region C, beyond x, where both velocity and thermal boundary layers are fully developed.

In Region A and Region B, the temperature profile for  $y \leq \delta_t$ may be assumed in the form

$$\frac{-t_{\theta}}{t_{q}} = \frac{3}{4} - \frac{y}{\delta_{t}} - \frac{1}{2} \left(\frac{y}{\delta_{t}}\right)^{2} + \left(\frac{y}{\delta_{t}}\right)^{3} - \frac{1}{4} \left(\frac{y}{\delta_{t}}\right)^{4} \quad (5)$$

Sector College, Howrah, India, Sector College, Howrah, India, Sector College, Howrah, India, Sector College, Howrah, India, 2L. Schiller, "Die Entwicklung der laminaren Geschwindig-MECHANICAL ENGINEERS. Manuscript received at ASME Keitsverteilung und ihre Bedeutung für Zähig-Keitsmessungen" ZAMM, vol. 2, 1922, pp. 96-106.





Roy, D. N., Laminar heat transfer in the inlet of a uniformly heated tube, Trans. ASME, J. Heat Transfer, vol. 84, p.425, 1965.



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Journal of Heat Transfer, p. 425, August, 1965

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From the continuity of flow, it follows

$$\delta^* = 2\sqrt{}$$

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$$x, y = \text{position coordinates as shown in Fig. 1.}$$
  
 $y/R = \text{dimensionless distance from the wall}$   
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3,

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Fig. 1

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a Uniformly Heated Tube

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<sup>2</sup>L. Schiller, "Die Entwicklung der laminaren Geschwindig-Keitsverteilung und ihre Bedeutung für Zähig-Keitsmessungen' ZAMM, vol. 2, 1922, pp. 96-106.

#### Heat Transfer Enhancement



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-Fig.

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inside radius and diameter of the tube position coordinates as shown in Fig. 1. dimensionless distance from the wall

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